

Ultra Clean Hydrogen From Biomass to Generate Combined Heat and Power using Fuel Cells

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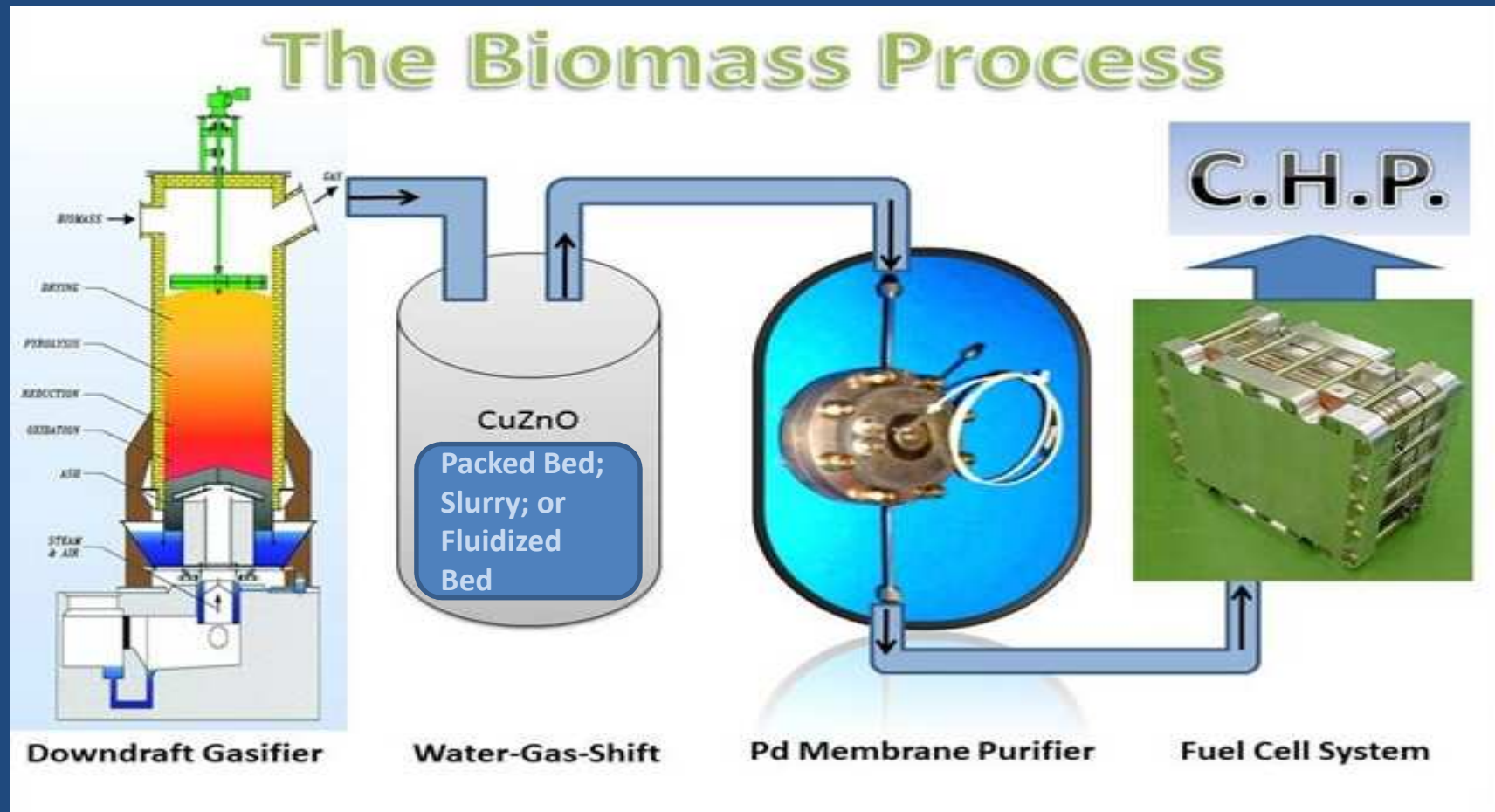
2 Brookhaven National Laboratory (BNL)

3 Stony Brook University

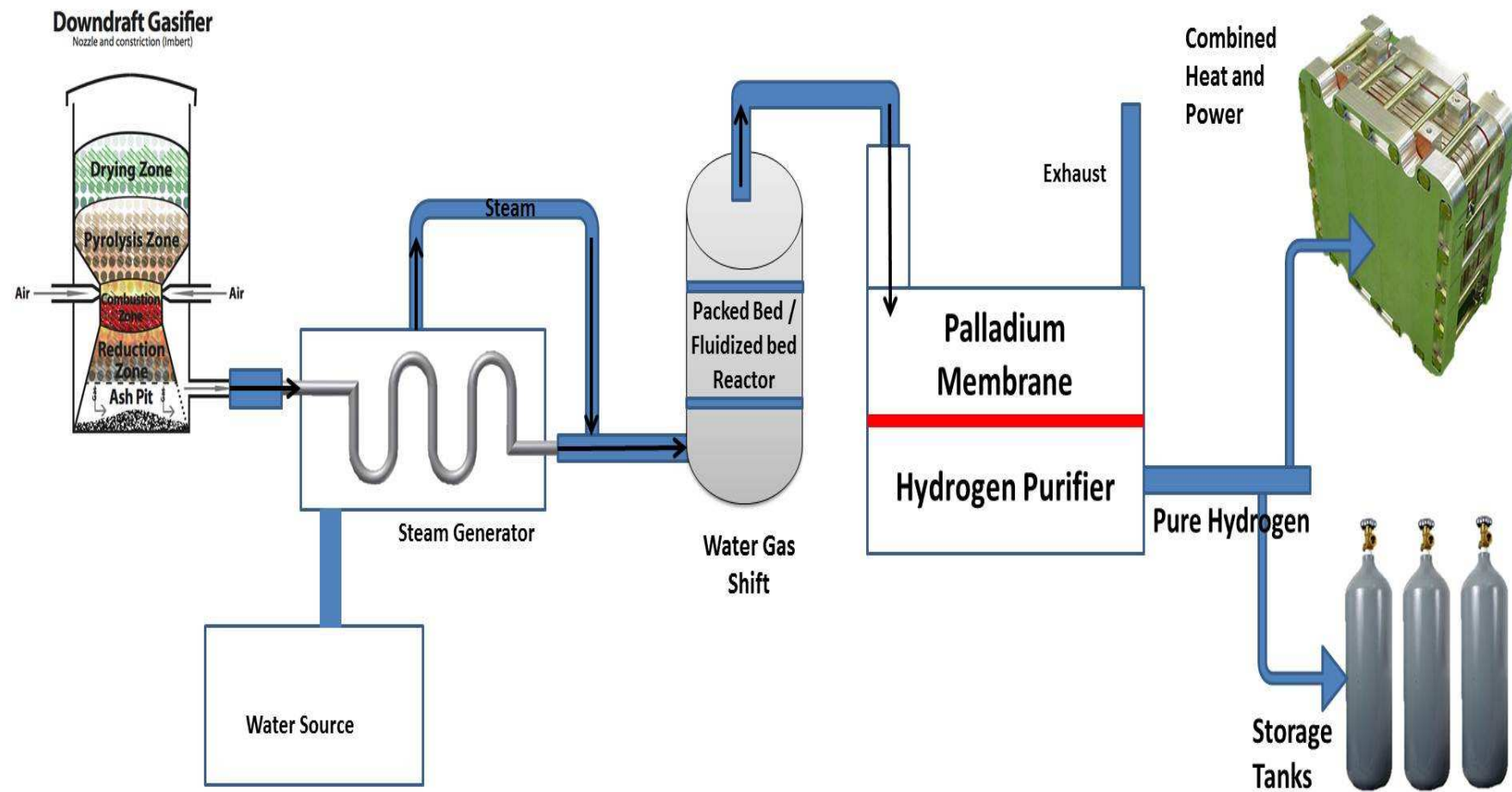
Biomass Energy

- *Excellent Potential for Economic Viability*
- *Renewable Energy Source*
- *Net Zero balance for Carbon Footprint*

General Presentation of the Hydrogen Generation from Biomass, Purification and Utilization Systems



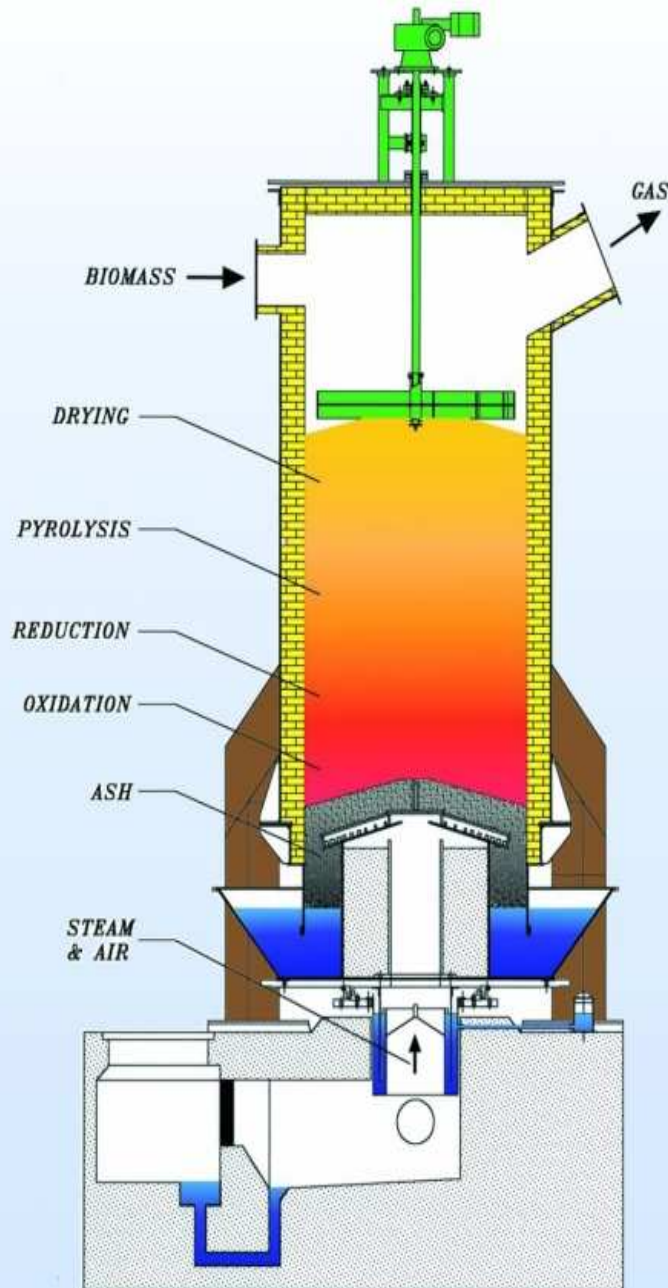
Detailed Biomass Hydrogen Cleanup and Separation Process



Updraft Gasifier

Farmingdale Gasifier

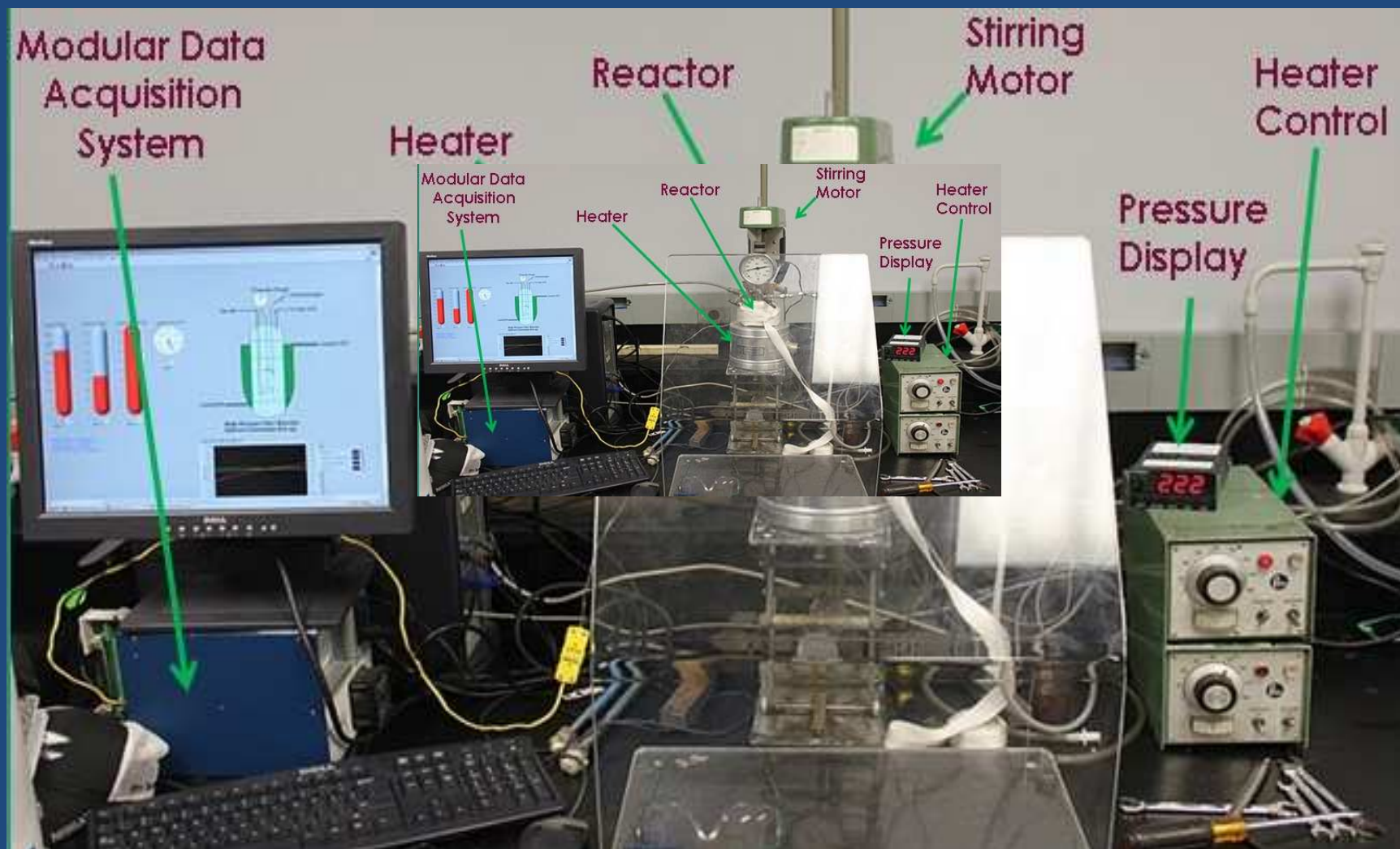
- Technical Specifications
- 10 kW
- Gasification fuel is wood chips with 15% water
- Syngas 50 m³/hr or 15 lbs/hr
- Wood Chip up to 40 lbs /hr
- 10 -25 lbs of air per hr
- Efficiency 70%
- Foot print 4 x 4 feet – height 5.5 feet



GEK v3.5 with Auger Feed Drying Bucket



Experimental Setup



Low Temperature Water Gas Shift (WGS)

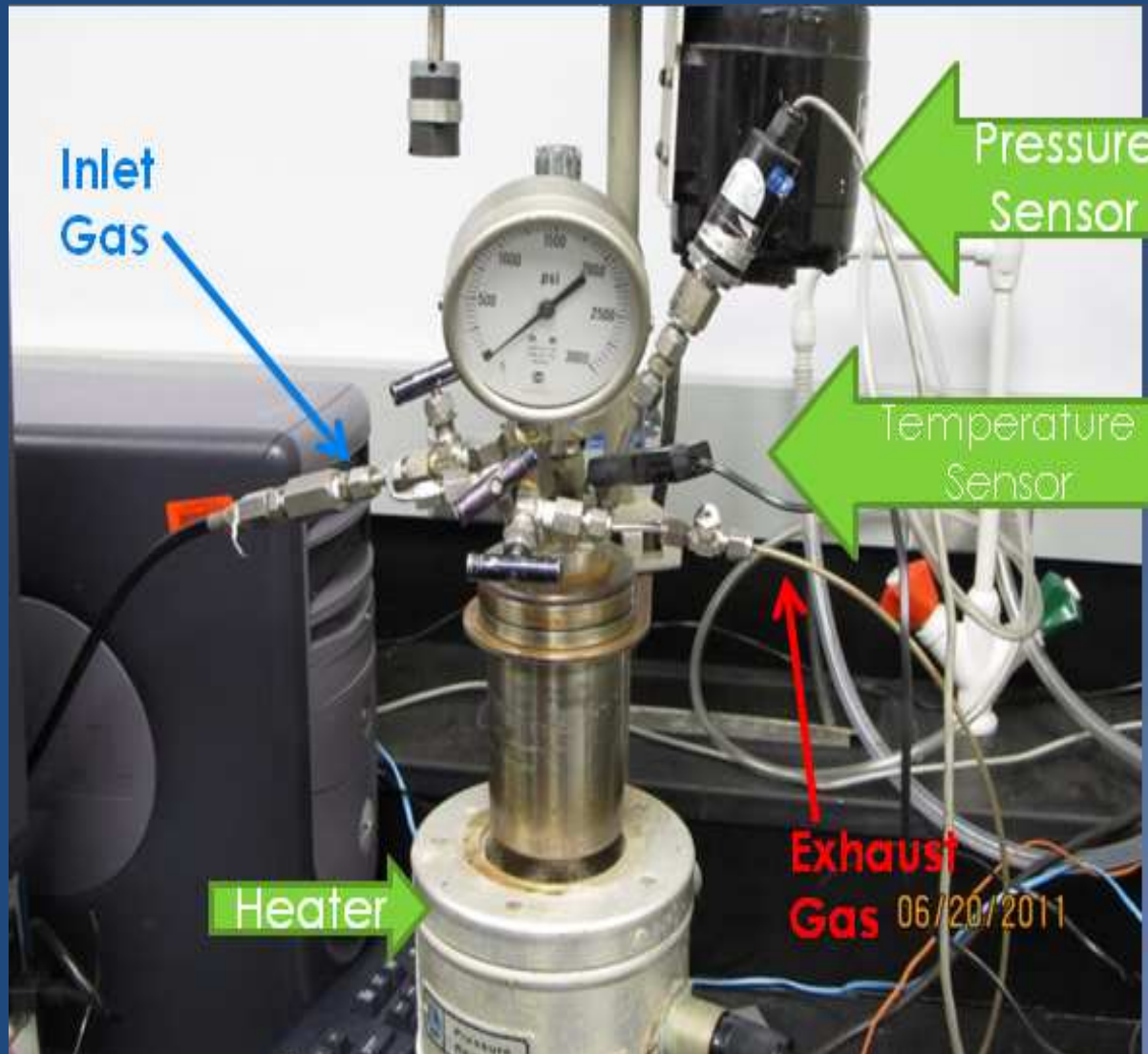
Low Temp Catalyst testing at 250 Degree C

- Copper Zinc Oxide
- Platinum Cerium Oxide (Ceria)
- Platinum Titanium Oxide
- Iron Chromium Oxide

Water Gas Shift Equation



Water Gas Shift (WGS) Reactor

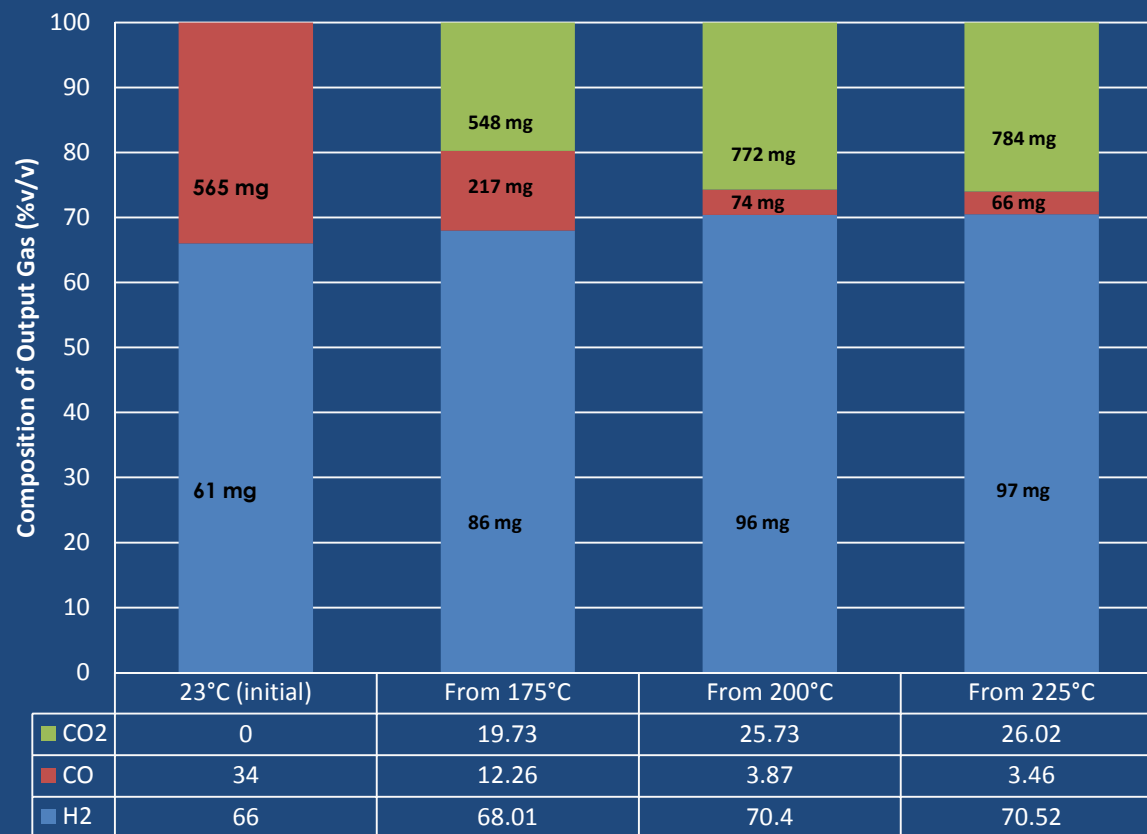


Closed Loop Reactor with Relatively Small Space Velocity and high Residence time

Slurry Mixture

- was composed of 2 grams of ground CuZnO catalyst, 70ml of Ethylflo-164 oil, 5ml of distilled H₂O, and 50psi pre-charge of Syngas composed of 34% CO and 66% H₂. Operation temperatures were 175°C, 200 °C, and 225 °C

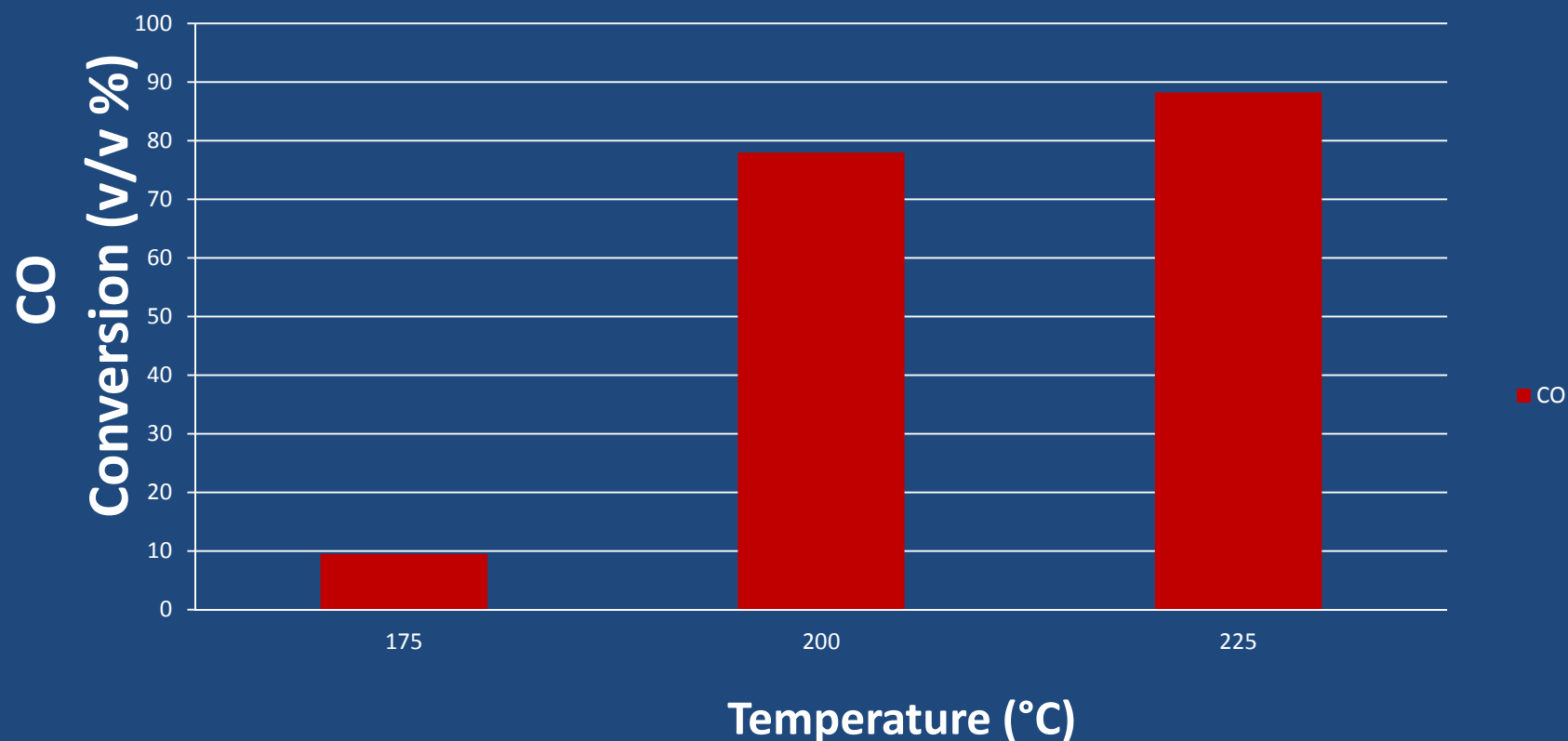
Effect of Temperature on Slurry CuZnO Catalyst Activity



This catalytic reaction was capable of bringing CO down from 34% to 3.46 % by volume and from 545 mg to 66 mg by weight

Carbon Monoxide (CO) Percentage Conversion for the CuZnO Catalyst at Different Temperature

CO Conversion at 225°C is almost 90%



Packed Bed Reactor Design

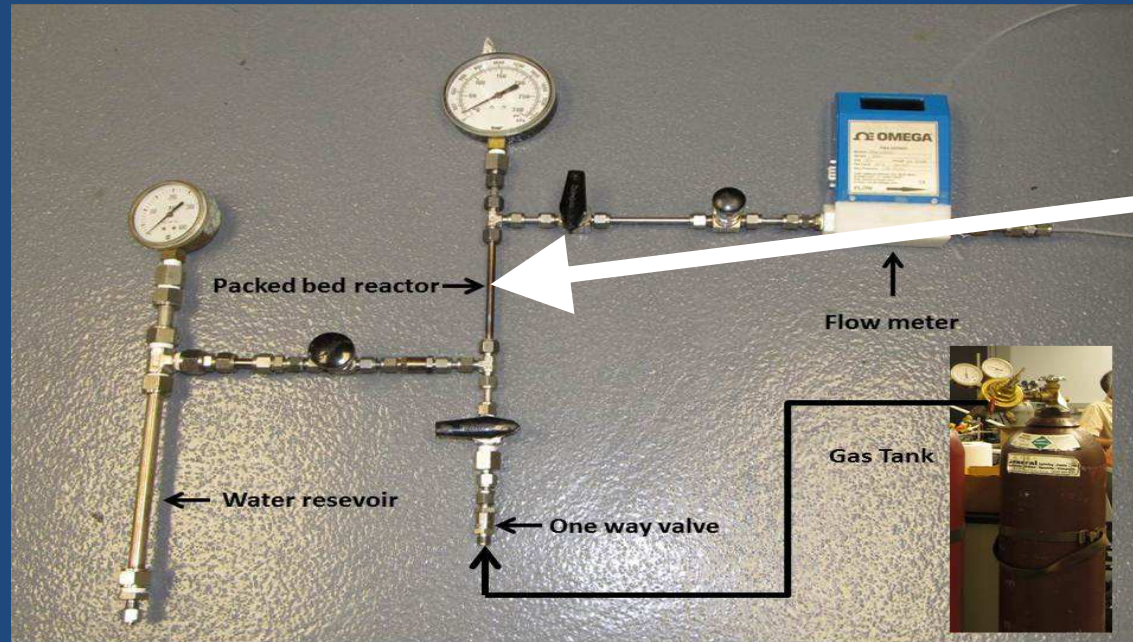


Figure 1: Experimental Apparatus



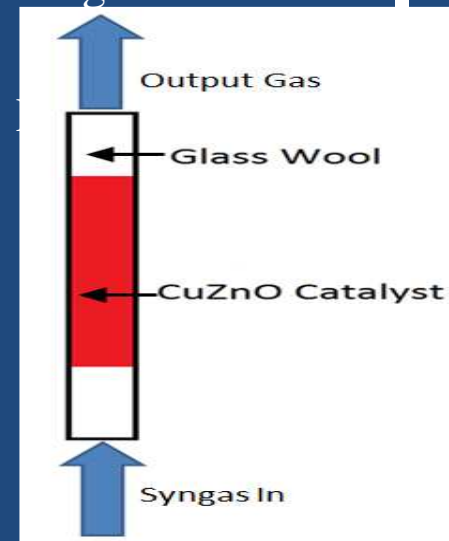
Temperature was controlled and monitored with a variable transformer and hand held digital temperature gage.



One way valve, used to prevent any feed back gas into the tank.

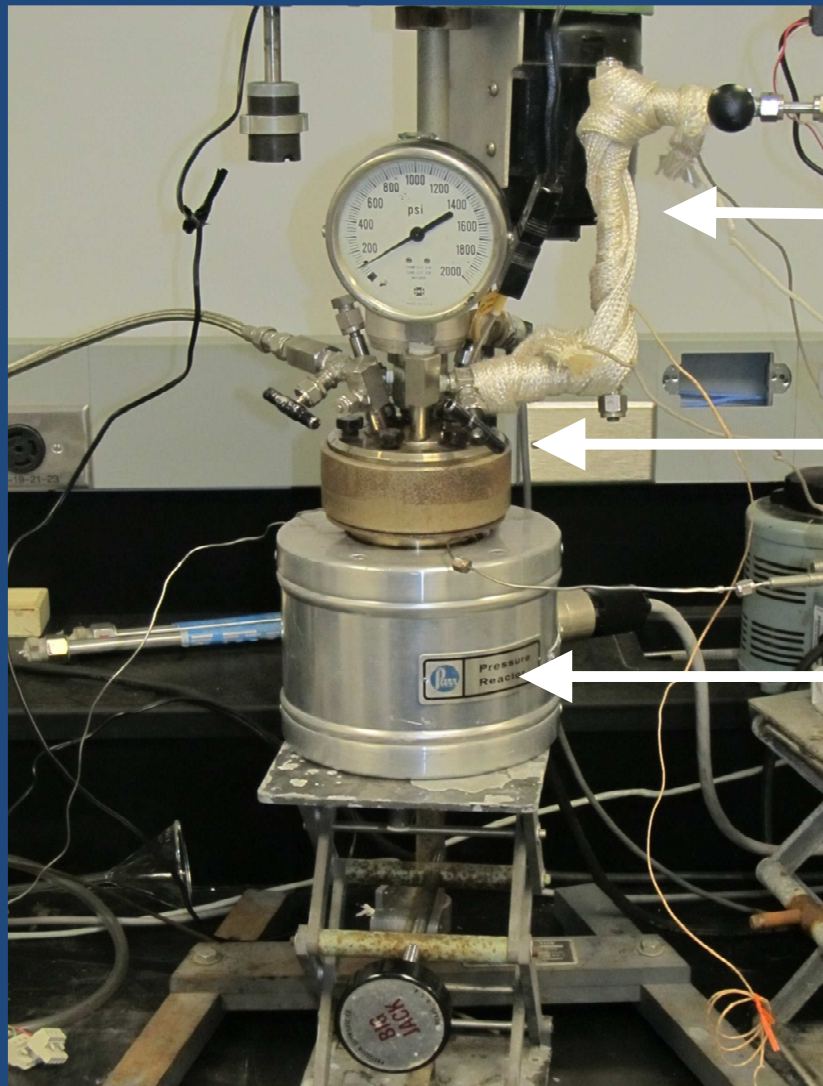


Figure 2:



Packed Bed Reactor

Packed Bed Reactor V2

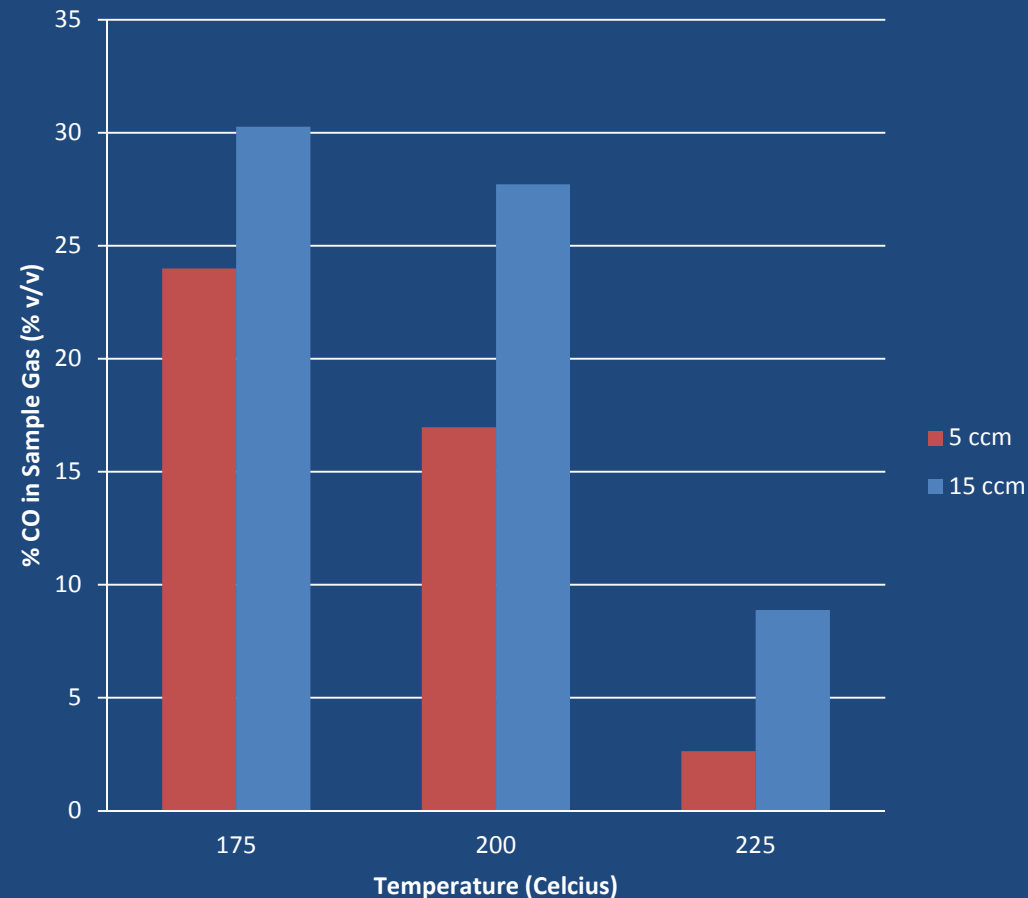


Packed bed
reactor
wrapped in
heating tape

Parr Bench
Top Reactor

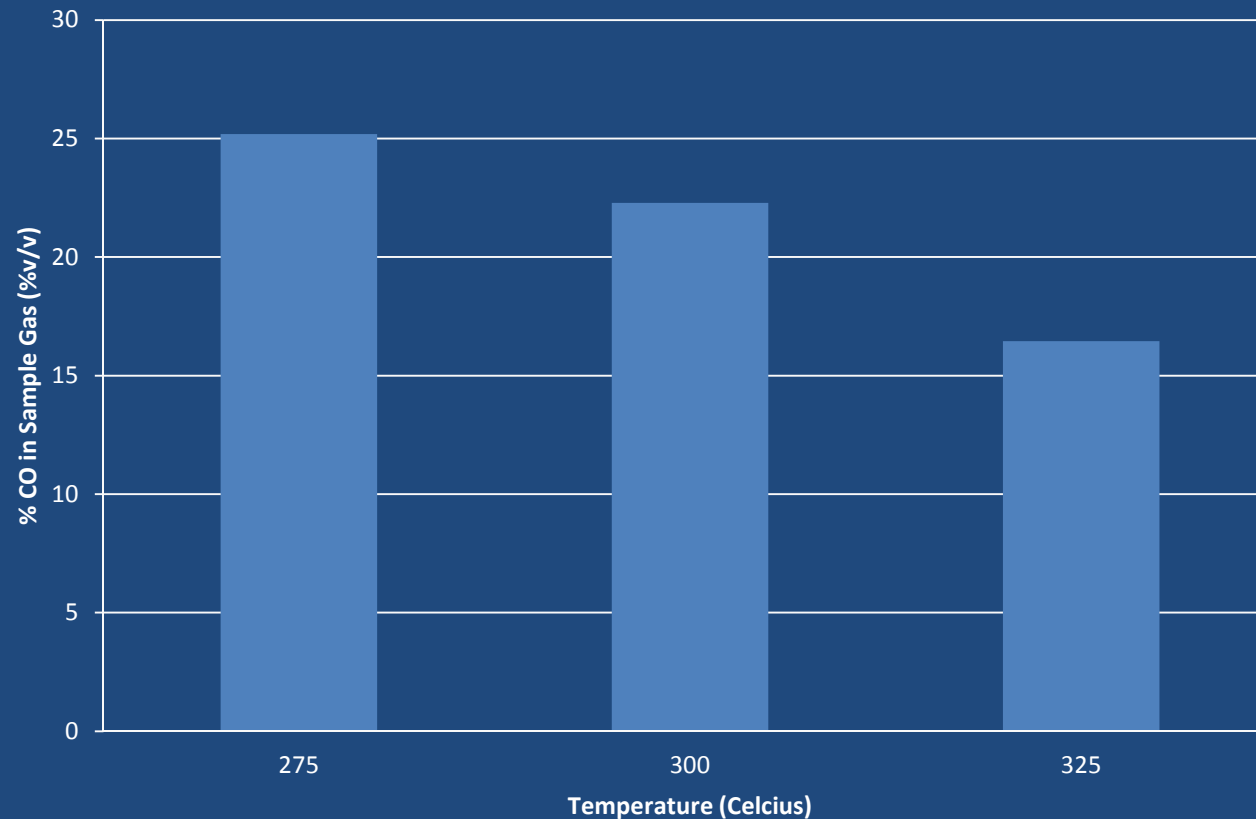
Heater

Effect of Flow Rate / Residence Time on Output Gas Composition Using Packed Bed CuZnO



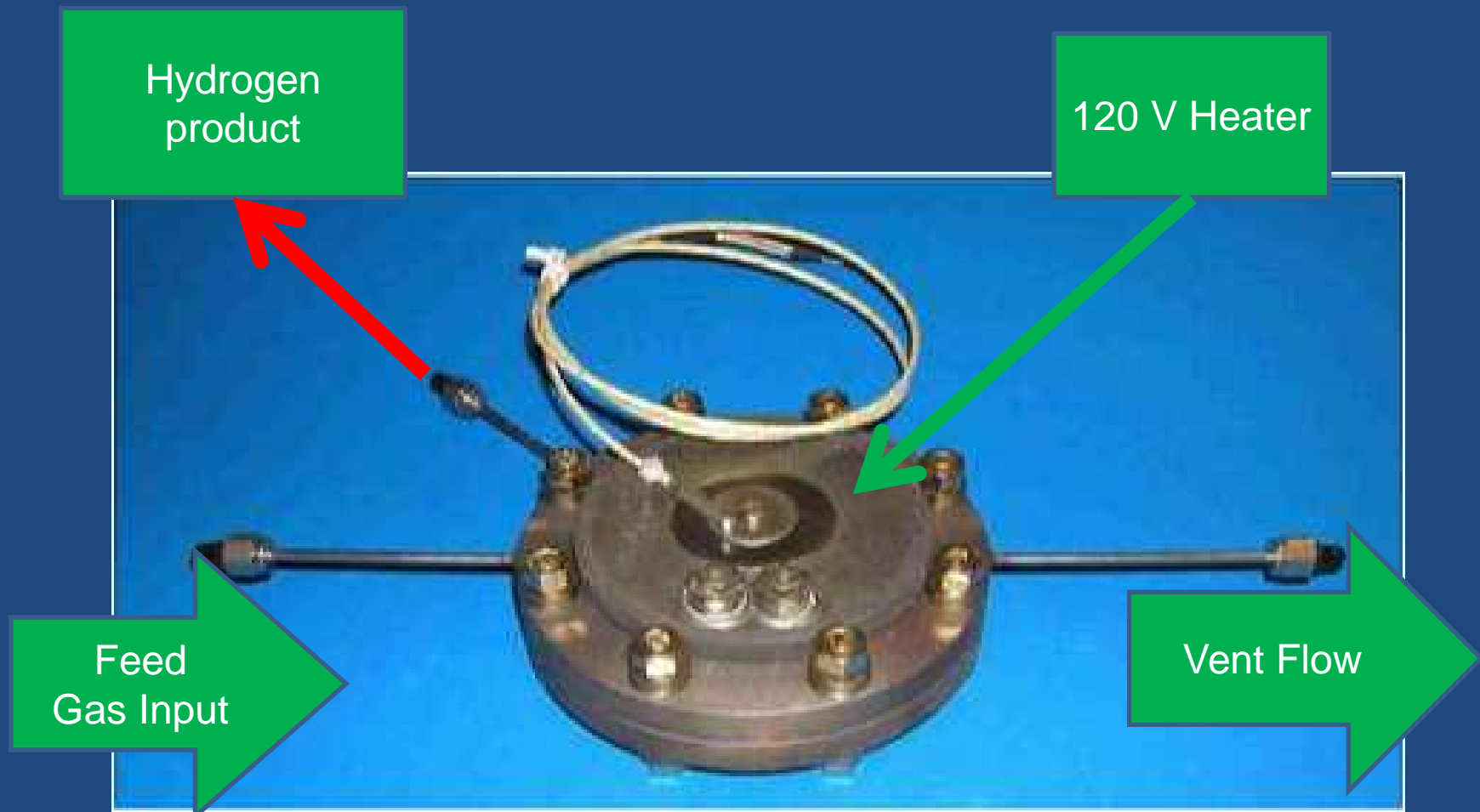
The outputs gas, after the WGS reaction at 225°C, the CO concentration was lowered to (2.64%) from 34% at flow rate of 5ccm and the CO concentration was lowered to (8.3%) from 34% at flow rate 15 ccm

Iron Chromium Oxide Performance in WGS Reaction at Various Temperatures in a Packed Bed Reactor



Initial CO concentration (34 %) in the input gases at room temp - output gases CO concentration , after the WGS reaction at all three temperatures

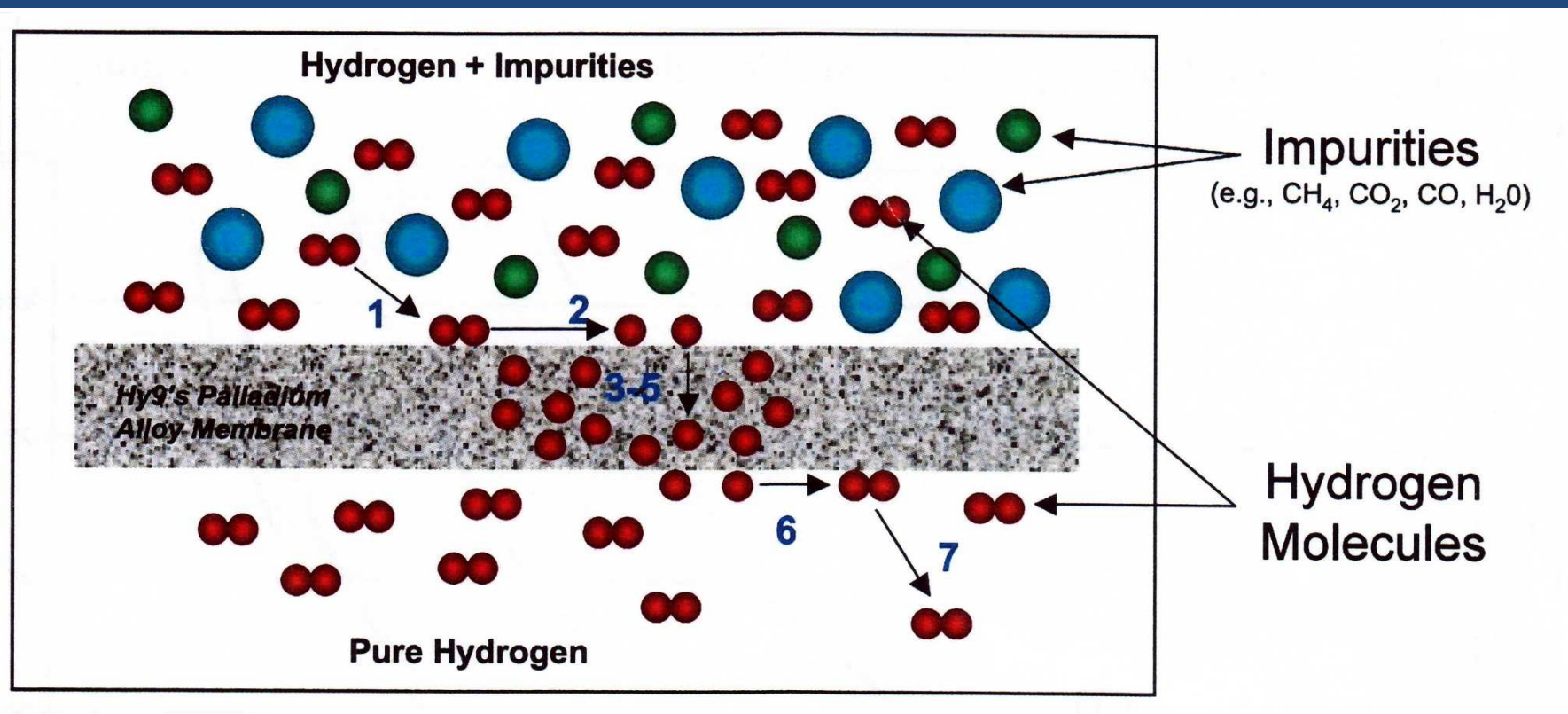
Testing Small Scale Hydrogen Purifier



Palladium Membrane Technology

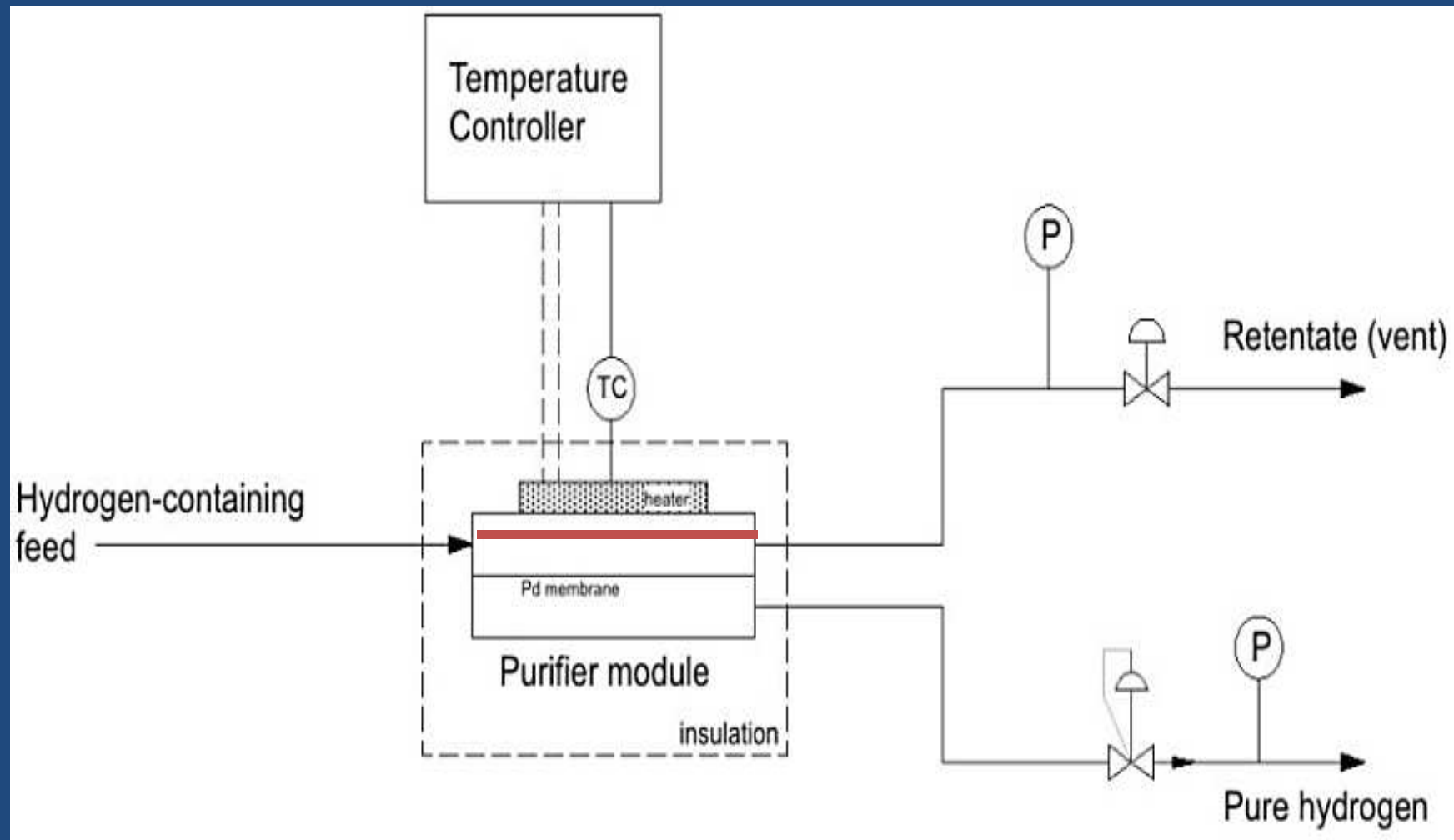
- How does the Palladium membrane purify the hydrogen?

– <http://www.hy9.com/membranepure.html>

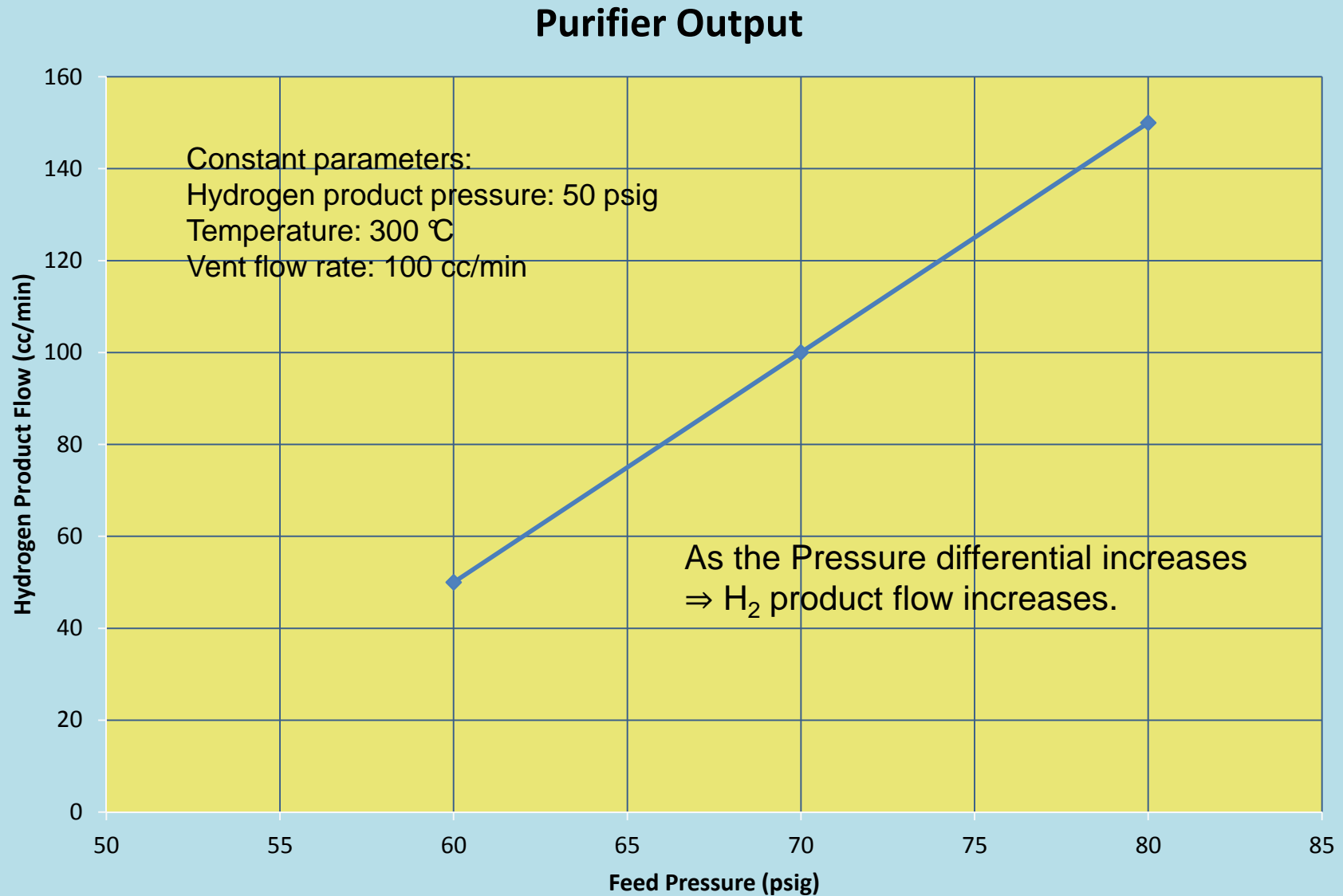


Palladium Membrane Purifier

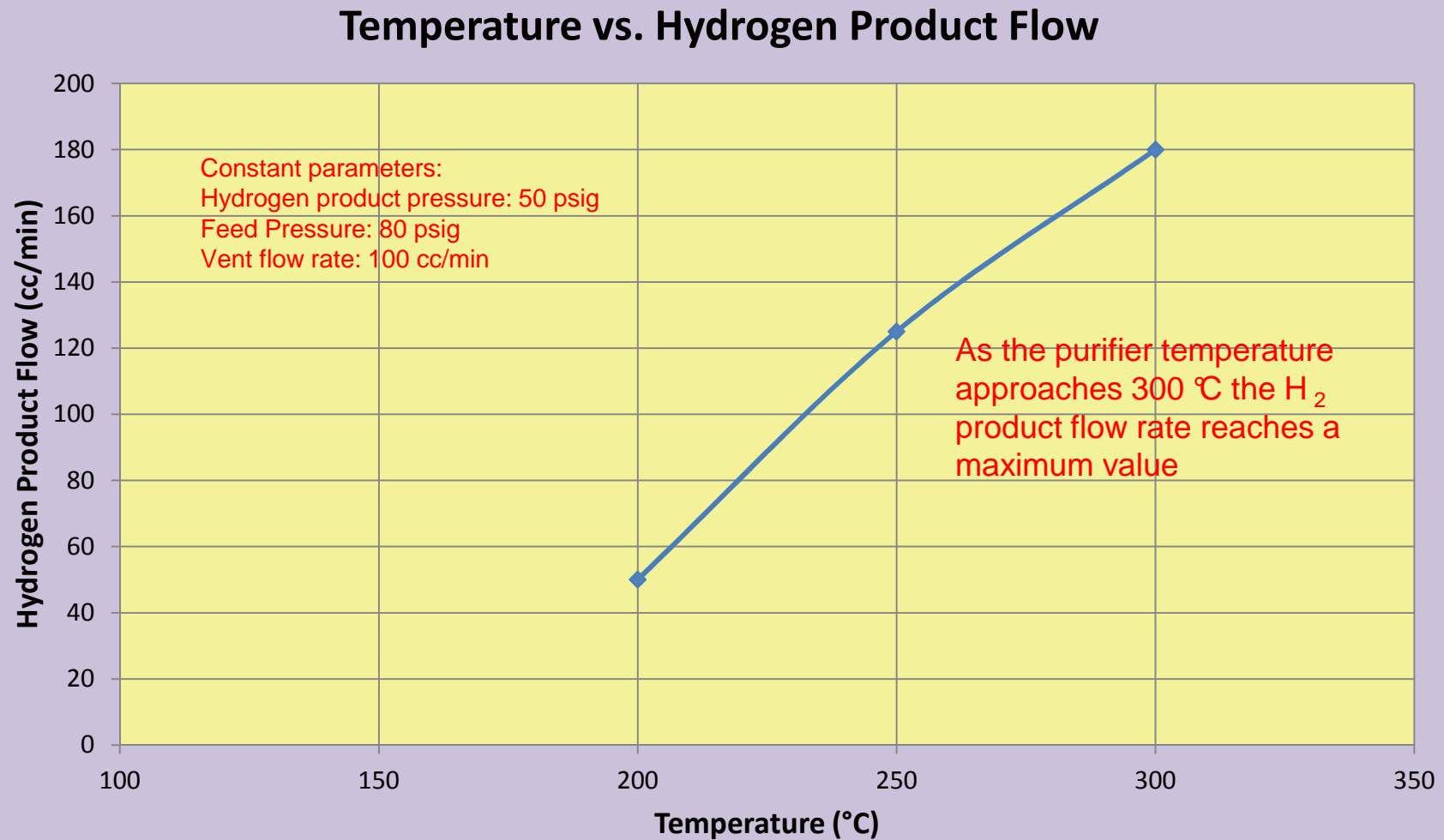
- The orientation of the palladium membrane in this hydrogen purifier is parallel with respect to the flow of the syngas.



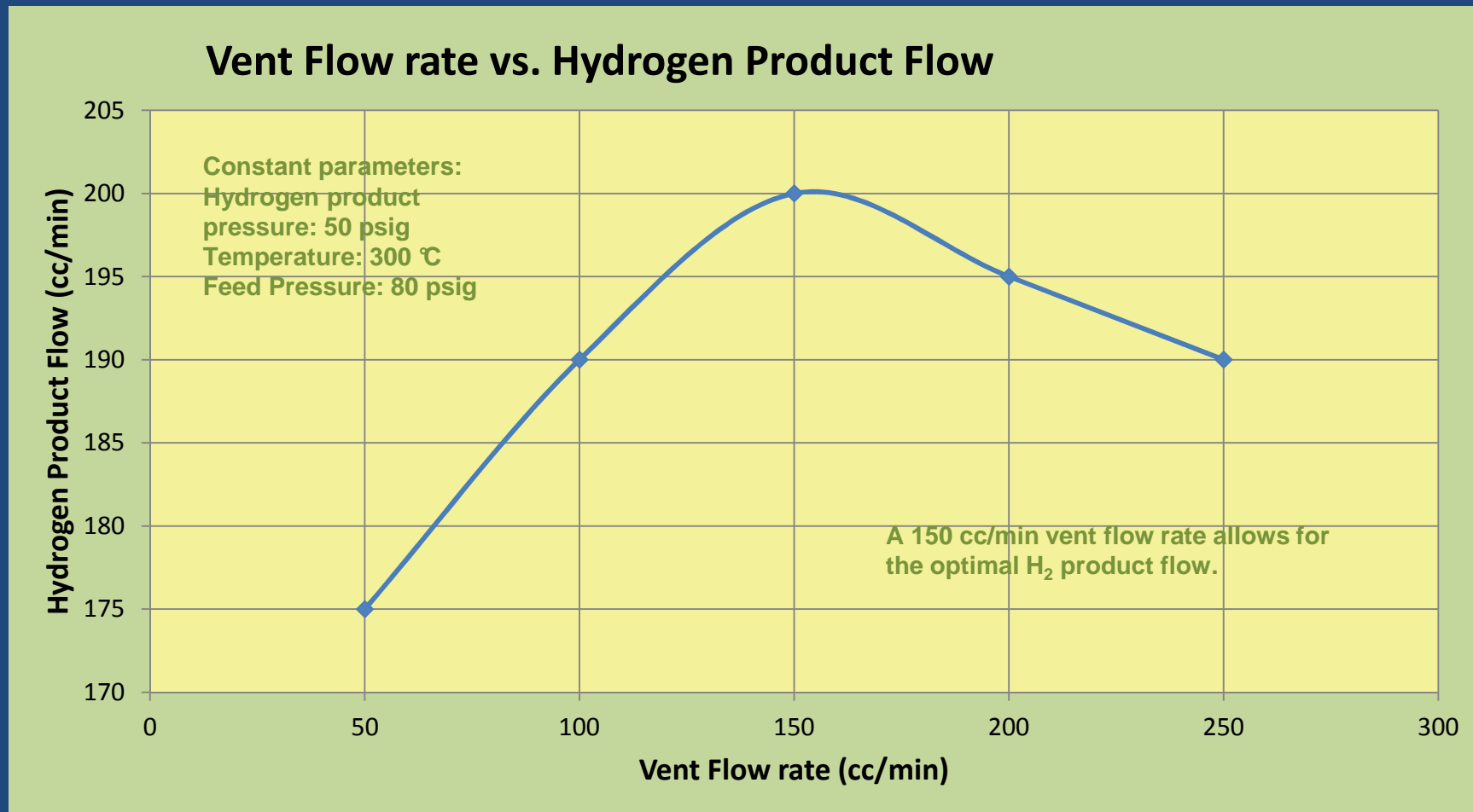
Hydrogen Purifier Experimental Results



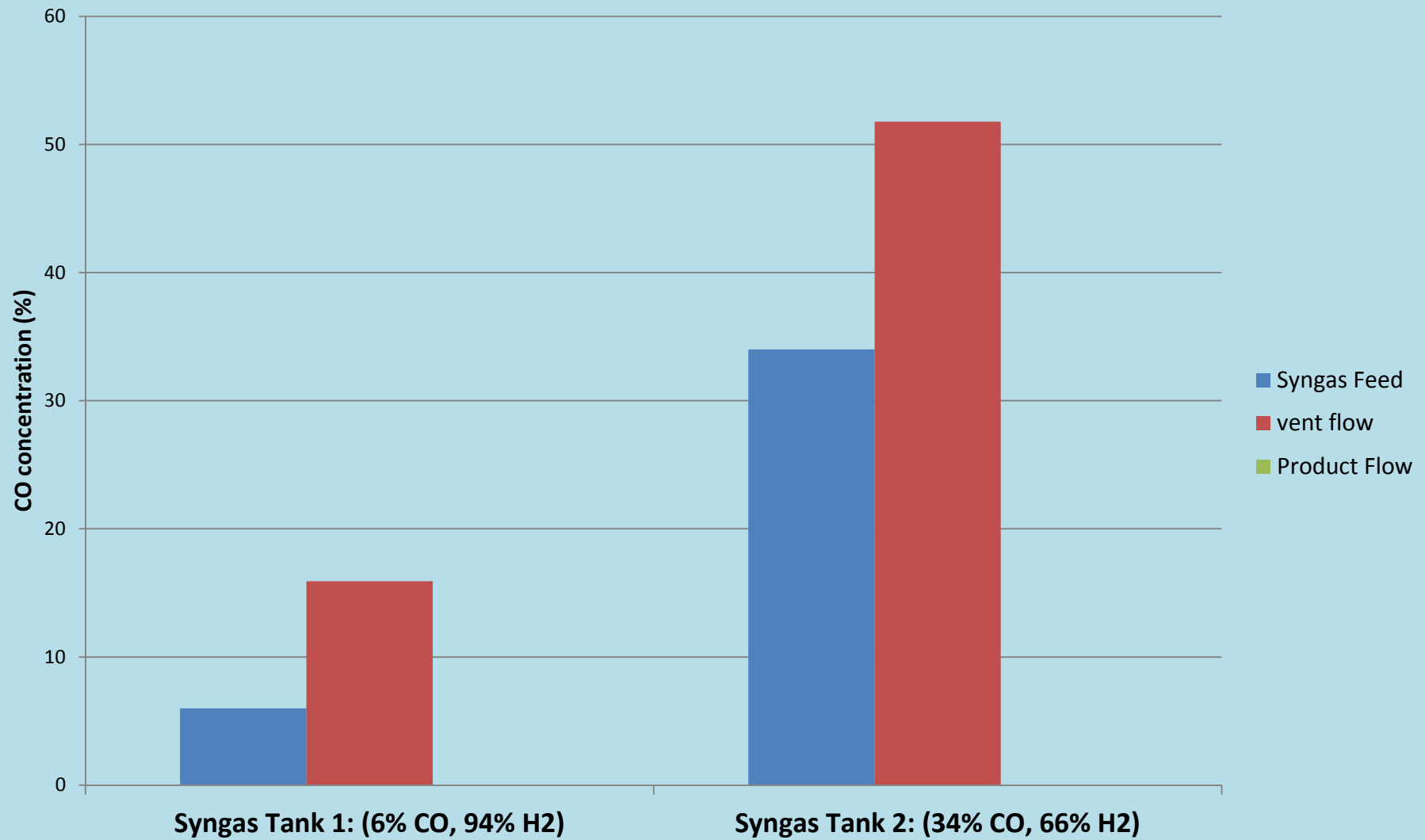
Effect of Temperature on H₂ Output



Effect of Vent Flow Rate on H₂ output

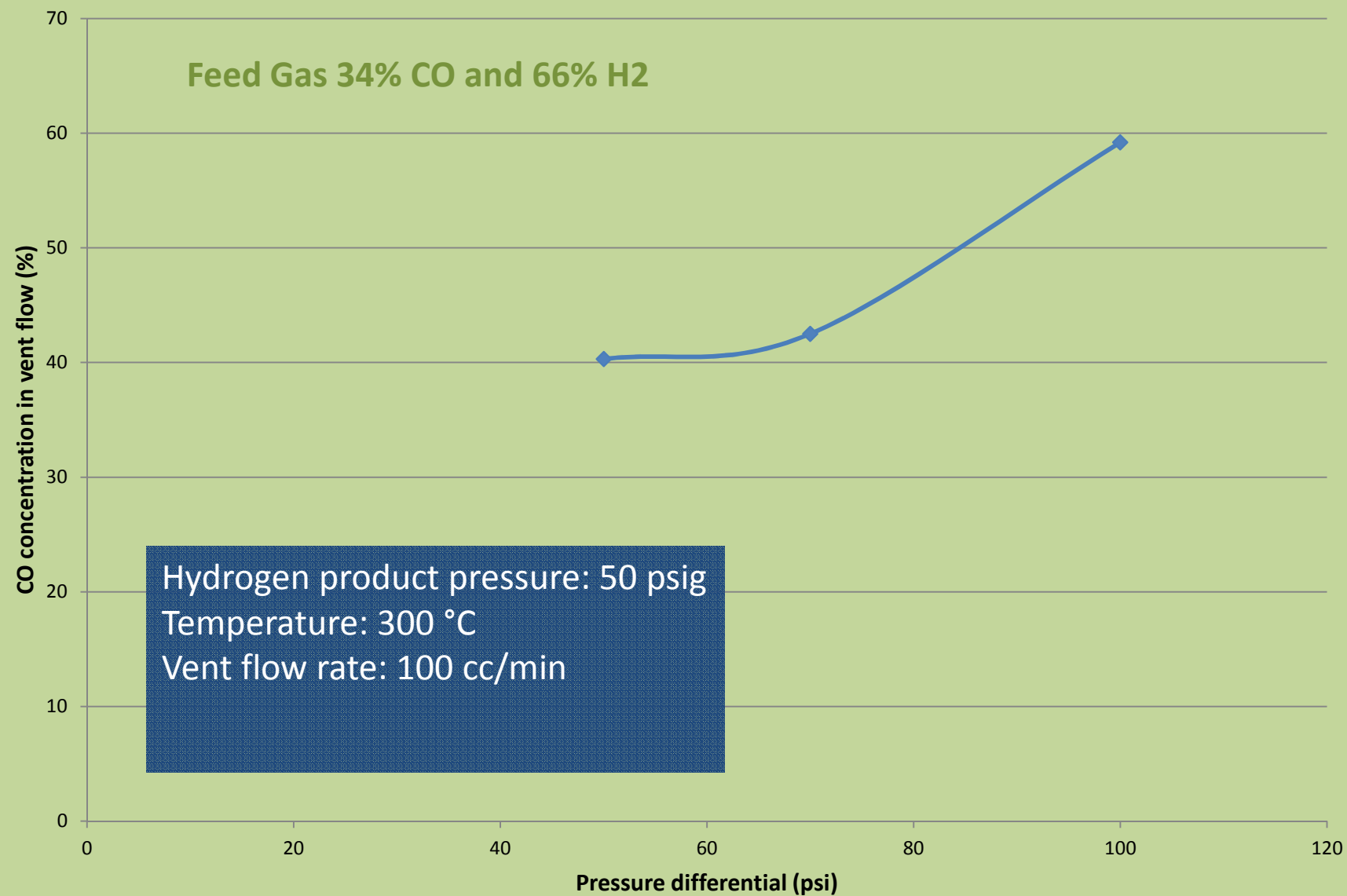


CO concentration Comparison



Pressure Differential vs. CO Concentration in Vent Flow

Feed Gas 34% CO and 66% H₂



Conclusions

- CuZnO Catalyst provided very promising results for both closed and open loop Water Gas Shift Reaction Systems
- CO was reduced from 34% to 3.46 % and 2.64% in closed and open loop Water Gas Shift Reaction Systems respectively
- Hydrogen Purification System provided 0% CO and 99.9999% pure H₂
- This Hydrogen Cleanup system is will poised for scale up to produce 75 SLM Pure H₂